

(19)



Europäisches Patentamt

European Patent Office

Office européen des brevets



(11)

**EP 0 537 968 B1**

(12)

**EUROPEAN PATENT SPECIFICATION**

(45) Date of publication and mention  
of the grant of the patent:  
24.01.1996 Bulletin 1996/04

(51) Int. Cl.<sup>6</sup>: **B01D 53/56**

(21) Application number: 92309288.6

(22) Date of filing: 13.10.1992

(54) **Nitrogen oxides decreasing apparatus for an internal combustion engine**

Einrichtung zur Minderung von Stickstoffoxiden in Rauchgasen aus Brennkraftmaschinen

Dispositif pour diminuer l'émission des oxydes d'azote des moteurs à combustion interne

(84) Designated Contracting States:  
**DE FR GB**

(30) Priority: 16.10.1991 JP 298252/91

(43) Date of publication of application:  
21.04.1993 Bulletin 1993/16

(73) Proprietor: **TOYOTA JIDOSHA KABUSHIKI  
KAISHA  
Aichi-ken 471 (JP)**

(72) Inventors:

- Oshima, Yujiro,  
c/o K. K. Toyota Chuo Kenkyusho  
Aichi-gun, Aichi-ken, 480-11 (JP)
- Muraki, Hideaki,  
c/o K. K. Toyota Chuo Kenkyusho  
Aichi-gun, Aichi-ken, 480-11 (JP)

- Yokota, Koji,  
c/o K. K. Toyota Chuo Kenkyusho  
Aichi-gun, Aichi-ken, 480-11 (JP)
- Nakanishi, Kiyoshi,  
c/o Toyota Jidosha K. K.  
Toyota-shi, Aichi-ken, 471 (JP)

(74) Representative: **Ben-Nathan, Laurence Albert et al  
London W1M 8AH (GB)**

(56) References cited:

**EP-A- 0 147 751                      EP-A- 0 380 143  
EP-A- 0 445 408**

- **DATABASE WPIL Derwent Publications Ltd.,  
London, GB; AN 81-44992D**

Note: Within nine months from the publication of the mention of the grant of the European patent, any person may give notice to the European Patent Office of opposition to the European patent granted. Notice of opposition shall be filed in a written reasoned statement. It shall not be deemed to have been filed until the opposition fee has been paid. (Art. 99(1) European Patent Convention).

## Description

The present invention relates to a nitrogen oxides (NOx) decreasing apparatus for an internal combustion engine. More specifically, the present invention relates to an exhaust gas purification system with a lean NOx catalyst capable of reducing NOx included in exhaust gas from an internal combustion engine, such as a so-called lean burn gasoline engine, a diesel engine, or a hydrogen engine, independently of a concentration of oxygen (O<sub>2</sub>) included in exhaust gas, that is, independently of an operating air-fuel ratio. Such an apparatus is for example described in EP-A-0147751.

As a method for decreasing NOx included in exhaust gas from an internal combustion engine, the following three methods are known:

- (1) to decrease NOx by using a three-way catalyst,
- (2) to decrease NOx by using combustion at excessively lean air-fuel ratios, and
- (3) to decrease NOx by using a lean NOx catalyst (as disclosed in JP-A-01139145). However, there are the following problems with these methods.

With method (1), the ratio of air to fuel supplied to an engine must be controlled to about 14.5, namely, the stoichiometric air-fuel ratio. If the air-fuel ratio is leaner than the stoichiometric air-fuel ratio, NOx cannot be decreased by the three-way catalyst. Contrarily, it is well known that to obtain good fuel economy, an engine should be operated at air-fuel ratios leaner than the stoichiometric air-fuel ratio, as shown in FIG. 2. Thus, NOx decrease and fuel economy are incompatible in method (1).

Method (2) seeks to combine NOx decrease with fuel economy by using a so-called lean burn engine. However, when the engine is operated at air-fuel ratios lean enough to decrease NOx, the combustion approaches a misfire limit, and driveability gets worse. To prevent this, an improvement has been proposed, wherein turbulences are generated within an engine cylinder so that the burning velocity is increased to thereby shift the misfire limit to the lean side. However, if the turbulences are excessive and the flow velocity becomes too high, formation of a flame core and propagation of the flame in an early period of combustion will be obstructed. Thus, there is a limit to this method. Also, another improvement has been proposed, wherein the air-fuel ratio distribution within an engine cylinder is controlled so that rich air-fuel mixtures are formed only in a region close to the ignition plug to produce easy ignition. However, as illustrated in FIG. 3, when the misfire limit is shifted to the lean side, the negative slope of the NOx concentration curve also is decreased. Thus, not much effect on NOx concentration can be expected.

Method (3) is intended to solve the above-described problems of item (2), more particularly, to operate an engine at air-fuel ratios slightly closer to the stoichiometric air-fuel ratio than the misfire limit and then to purify

the insufficiently decreased NOx by using a zeolite-type lean NOx catalyst. This method has the potential to provide a clean system that also has good fuel economy. However, since the lean NOx catalyst can operate only under oxidizing exhaust gas conditions and is usually exposed to high temperatures, it is difficult to obtain both a sufficiently high NOx conversion by the lean NOx catalyst and durability of the catalyst.

As will be understood from the above, problems of practical use exist with any conventional NOx decreasing method.

Lean burn gasoline engines as well as diesel engines include excess O<sub>2</sub> in the exhaust gas, that is, they are operated under oxidizing gas conditions. The leaner the air-fuel ratio, the greater is the concentration of O<sub>2</sub> included in the exhaust gas. A catalyst which reduces NOx under oxidizing gas conditions is defined as a lean NOx catalyst, which is usually composed of a noble metal-type catalyst or a zeolite-type catalyst. The lean NOx catalyst has an NOx conversion versus temperature characteristic as shown in FIG. 4. At temperatures above 350°C, mainly reduction of NOx by HC occurs, while at low temperatures below 250 - 350°C, reduction of NOx by hydrogen (H<sub>2</sub>) occurs, wherein NOx purification by H<sub>2</sub> is possible.

However, since the lean NOx catalyst is usually installed in or near an engine exhaust manifold in a conventional exhaust system, the temperature to which the catalyst is exposed is as high as 800 - 900°C. Further, since the lean burn engine is operated at above stoichiometric air-fuel ratios, almost no H<sub>2</sub> remains in the exhaust gas. Therefore, the NOx reduction characteristic of a lean NOx catalyst at low temperatures below 250 - 350°C has not been used in a conventional lean burn gasoline engine or diesel engine.

An object of the invention is to provide an NOx decreasing apparatus for an internal combustion engine (a lean burn gasoline engine, a diesel engine, or a hydrogen engine), which can effectively reduce NOx included in exhaust gas even under oxidizing gas conditions, independently of a concentration of O<sub>2</sub> included in the exhaust gas, without deteriorating a fuel economy characteristic of the engine.

The invention provides an NOx decreasing apparatus in accordance with Claim 1.

In the apparatus of the invention, methanol or hydrocarbons are led to the reforming catalyst, where the methanol or hydrocarbons are reformed to generate H<sub>2</sub>. The generated H<sub>2</sub> is supplied into the exhaust conduit of the engine at the inlet side of the NOx reduction catalyst and is mixed with NOx-containing exhaust gas from the engine. The NOx reduction catalyst causes H<sub>2</sub> and NOx to react with each other at low temperatures to reduce NOx. Since NOx is reduced through reaction with H<sub>2</sub> independently of a concentration of O<sub>2</sub> included in exhaust gas, the air-fuel ratio can be freely determined from the viewpoint of good combustion and fuel economy without having to achieve minimum generation of NOx.

As a result, a high fuel economy and good driveability can be maintained.

The above-described object and other objects, features, and advantages of the present invention will become more apparent and will be more readily appreciated from the following detailed description of the preferred embodiments of the invention taken in conjunction with the accompanying drawings, in which:

FIG. 1 is a schematic system diagram illustrating a basic arrangement of an NOx decreasing apparatus for an internal combustion engine in accordance with the present invention;

FIG. 2 is a graphical representation of a specific fuel consumption versus air-fuel ratio characteristic;

FIG. 3 is a graphical representation of an NOx and specific fuel consumption versus air-fuel ratio characteristic;

FIG. 4 is a graphical representation of an NOx conversion versus inlet gas temperature characteristic;

FIG. 5 is a graphical representation of an NOx conversion versus ratio of amount of supplied H<sub>2</sub> to amount of NOx characteristic;

FIG. 6 is a schematic system diagram of an apparatus in accordance with a first embodiment of the invention;

FIG. 7 is an enlarged cross-sectional view of an H<sub>2</sub> generator of the apparatus of FIG. 6;

FIG. 8 is a still further enlarged cross-sectional view of an inlet end portion of the H<sub>2</sub> generator of FIG. 7;

FIG. 9 is a schematic system diagram of an apparatus in accordance with a second embodiment of the invention;

FIG. 10 is an enlarged side view of one embodiment of an H<sub>2</sub> mixer and NOx reduction catalytic converter according to the invention;

FIG. 11 is a graphical representation comparing NOx converting characteristics of a pellet-type catalyst and a monolithic catalyst used in the NOx reduction catalytic converter of FIG. 10;

FIG. 12 is a partial cross-sectional view of a pellet-type catalyst for use in the NOx reduction catalytic converter of FIG. 10;

FIG. 13 is a partial cross-sectional view of a monolithic catalyst for use in the NOx reduction catalytic container of FIG. 10;

FIG. 14 is a further enlarged cross-sectional view of an H<sub>2</sub> mixer for use in the apparatus of FIG. 10;

FIG. 15 is a cross-sectional view of the mixer taken along line 15-15 of FIG. 14;

FIG. 16 is a schematic cross-section illustrating a dimensional relationship between a diameter d of an H<sub>2</sub> injection nozzle and a diameter D of an exhaust conduit in the apparatus of FIG. 14;

FIG. 17 is a cross-sectional view of another mixer for use in the apparatus of FIG. 10;

FIG. 18 is a cross-sectional view of the mixer taken along line 18-18 of FIG. 17;

FIG. 19 is a graphical representation of an NOx conversion versus inlet gas temperature characteristic of an apparatus in accordance with a fourth embodiment of the invention;

FIG. 20 is an enlarged partial cross-sectional view of another embodiment of an H<sub>2</sub> mixer and NOx reduction catalytic converter according to the invention;

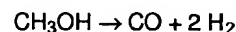
FIG. 21 is a cross-sectional view of the apparatus of the embodiment of FIG. 20 taken along line 21-21; and

FIG. 22 is a partial cross-sectional view of still another embodiment of an H<sub>2</sub> mixer and NOx reduction catalytic converter according to the invention.

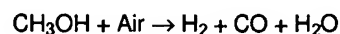
With reference to FIG. 1, in an NOx decreasing apparatus for an internal combustion engine in accordance with the present invention, an H<sub>2</sub> generator 102 for generating H<sub>2</sub> and supplying the generated H<sub>2</sub> to an exhaust conduit 101 of an engine 100 includes a reforming catalytic converter 102 containing a reforming catalyst 1. The type of reforming catalyst 1 is selected according to the kind of fuel used in the engine.

More particularly, in an engine using methanol as fuel, the following three types of reforming catalysts can be used:

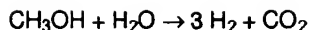
(1) At least one metal selected from the group consisting of noble metals such as palladium (Pd) and platinum (Pt), and transition metals such as copper (Cu), chrome (Cr), and nickel (Ni), is used as catalyst metal of the reforming catalyst. Methanol is evaporated by heat of the exhaust gas and is reformed at the reforming catalyst to generate H<sub>2</sub>. The temperature of an inlet portion of the reforming catalyst is maintained at about 300°C. The reaction at the reforming catalyst is as follows:



(2) A Cu-Ni-Cr/alumina catalyst (Cu-Ni-Cr is deposited onto a carrier of alumina) is used as the reforming catalyst. Methanol fuel is evaporated and is mixed with air. The mixture is led to the reforming catalyst where the methanol is partially-oxidized to generate H<sub>2</sub>. The catalyst temperature is maintained at 400 - 500°C by controlling the amount of air supplied to the methanol. The reaction at the reforming catalyst is as follows:



(3) Cu-Mn or Cu-Zn is used as the reforming catalyst. Water vapor, air, or mixture of methanol and water is added to methanol fuel to reform the fuel to generate H<sub>2</sub>. The catalyst temperature is controlled to about 250°C. The reaction at the reforming catalyst is as follows:



Further, in an engine using hydrocarbons (HC) such as LPG (liquefied petroleum gas) and natural gas as fuel, at least one kind of metal selected from the group consisting of Ni, Co (cobalt), and Rh (rhodium) is used as the reforming catalyst. The fuel is reformed at 300 - 800°C. Water vapor, air, or water from a water tank is added to the HC fuel to reform the HC fuel and to generate H<sub>2</sub>. The catalyst is maintained at a respective temperature according to the kind of catalyst used. Usually, methane is generated at low temperatures and CO (carbon monoxide) is generated at high temperatures. The reactions at the reforming catalyst are as follows:

|                                                                            |             |
|----------------------------------------------------------------------------|-------------|
| HC + H <sub>2</sub> O → H <sub>2</sub> + CH <sub>4</sub> + CO <sub>2</sub> | 300 - 500°C |
| HC + H <sub>2</sub> O → H <sub>2</sub> + CO + CO <sub>2</sub>              | 800°C       |
| HC + Air → H <sub>2</sub> + CO                                             | 800°C       |
| HC + EGR gas → H <sub>2</sub> + CO                                         | 700°C       |

In the NOx decreasing apparatus for an internal combustion engine in accordance with the invention, an NOx sensor 6 is installed in the exhaust conduit 101 connected to the internal combustion engine 100 to detect an NOx concentration of the exhaust gas, and an intake air sensor 5 is installed in an intake conduit 108 to detect a total amount of gas. In a controller 7 (electronic control unit), an amount of NOx is calculated from the output of the NOx sensor 6 and the output of the intake air flow sensor 5, and the amount of H<sub>2</sub> to be supplied to purify the calculated amount of NOx is determined. The amount of exhaust gas supplied to the reforming catalytic converter or the amounts of air and fuel supplied to the reforming catalytic converter to partially oxidize the fuel may be controlled in accordance with the determined amount of required H<sub>2</sub>.

Alternatively, the amount of NOx in the exhaust gas may be predicted from the outputs of the usual sensors for detecting the engine operating conditions such as an engine speed sensor, an intake pressure detecting sensor, and a throttle valve opening degree detecting sensor or a fuel injection detecting sensor of a fuel pump. The amount of fuel supplied to the reforming catalytic converter may be controlled corresponding to the predicted NOx amount.

Furthermore, in the NOx decreasing apparatus of the invention, a mixer is installed to evenly mix the supplied H<sub>2</sub> with exhaust gas, and a muffler may be constructed integrally with the NOx reduction catalyst to make a compact assembly of the muffler and the NOx reduction catalytic converter.

In more detail, a basic system of the NOx decreasing apparatus for an internal combustion engine in accord-

ance with the present invention is illustrated in FIG. 1. A first feature of the invention is that NOx reduction by H<sub>2</sub> is performed at all air-fuel ratios at low temperatures. A second feature of the invention is that a reforming device to reform fuel to generate H<sub>2</sub> is included in the system. A third feature of the invention is that the H<sub>2</sub> generation is controlled according to the amount of NOx included in the exhaust gas, that is, according to the engine operating conditions, so that the H<sub>2</sub> is supplied to a NOx reduction catalyst in the proper molar amount.

As illustrated in FIG. 1, the NOx reduction catalyst 2 is disposed at a downstream part of the exhaust conduit 101 in or near a muffler 3. If the NOx reduction catalyst were disposed upstream at a high temperature position, H<sub>2</sub> would react with O<sub>2</sub> and the selective reaction of H<sub>2</sub> with NOx would not occur.

A conduit 103 branches from a fuel conduit 104 connected to a fuel tank 105 and connects via a flow control valve 106 to the reforming catalytic converter 102 containing the reforming catalyst 1. An H<sub>2</sub> conduit 107 connects the reforming catalytic converter to the exhaust conduit upstream of the NOx reduction catalyst 2 so that the generated H<sub>2</sub> is supplied to an inlet side of the NOx reduction catalyst 2. In order to supply H<sub>2</sub> in molar proportion to the amount of NOx, the intake air sensor 5 is installed in the intake conduit 108 of the engine 100 and the NOx sensor 6 is installed in the exhaust conduit 101 of the engine to detect the concentration of NOx included in the exhaust gas. The amount of NOx included in the exhaust gas is calculated by the controller 7 based on the outputs of the sensors 5 and 6, and the amount of H<sub>2</sub> required to purify that amount of NOx is calculated by the controller 7.

To cause the H<sub>2</sub> generator to generate H<sub>2</sub> by the amount calculated, the amount of fuel to be supplied to the reforming catalytic converter, the amount of exhaust gas to heat the reforming catalytic converter, and the amount of air to be supplied to the reforming catalytic converter in the case where fuel is partially oxidized are controlled. In this connection, the amount of exhaust gas to heat the reforming catalytic converter is controlled by an exhaust bypass valve 110 installed in a bypass conduit 111. The air flow to the reforming catalytic converter is controlled by an air control valve 109.

FIG. 5 shows curves of NOx conversion versus ratio of H<sub>2</sub> to NOx. When H<sub>2</sub> is supplied at the ratio that H<sub>2</sub> ; NOx = 2 ; 1, all NOx will be reduced as shown by the theoretical line in FIG. 5, if the NOx and the supplied H<sub>2</sub> react completely with each other. However, since NOx and H<sub>2</sub> will not react completely with each other, the actual conversion will be as shown by the experimental curve in FIG. 5. At H<sub>2</sub>/NOx ratio less than 2.0, the experimental curve is positioned to the left of the theoretical line. This is because water vapor included in the exhaust gas is transformed into H<sub>2</sub> on the noble metal-type catalyst. Thus, more H<sub>2</sub> than the amount supplied from the reforming catalytic converter is available to react with the NOx.

In accordance with the invention, a mixer for mixing the supplied H<sub>2</sub> with exhaust gas is installed on an inlet side of the NOx reduction catalyst. In some embodiments of the invention, the reforming catalytic converter is installed downstream of an oxidation catalyst disposed at an outlet of an exhaust manifold of the engine, and the NOx reduction catalyst is installed in or downstream of the muffler so that the catalysts are maintained at respective optimum temperatures.

In other embodiments of the invention, an HC oxidation device for oxidizing HC and CO, such as an oxidation catalyst, a three-way catalyst, and an exhaust reactor is installed in a portion of the exhaust conduit close to the exhaust manifold, and Pt-zeolite catalyst (where Pt is deposited on zeolite) is used as the lean NOx catalyst. Further, the NOx reduction catalytic converter and the exhaust muffler are integrally constructed into a single assembly in which the NOx reduction catalyst is provided with a muffler function.

Further, in a diesel engine, a soot trapper or an unburned HC oxidizing device may be provided upstream of the NOx reduction catalyst. Furthermore, the present invention may be applied not only to a lean burn gasoline engine and a diesel engine but also to a hydrogen engine where hydrogen gas is used as fuel. In the case of a hydrogen engine, an H<sub>2</sub> generator is not required and a portion of the H<sub>2</sub> fuel can be supplied to an inlet side of the NOx reduction catalyst.

These embodiments of the invention will be explained in more detail below.

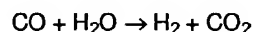
FIG. 6 illustrates a first embodiment of the invention where the system of the invention is applied to a lean burn gasoline engine 112 with an engine displacement of 1 liter. The engine 112 of the first embodiment is operated at excess air ratios of 0.95 - 1.0 (slightly rich or just a stoichiometric air-fuel ratio) in an idling condition, at excess air ratios of 0.8 - 1.0 (rich) in a full load condition and a rapid acceleration condition, and at excess air ratios of 1.2 - 1.8 in the remaining engine operating conditions. An oxidation catalyst 9 is installed in an exhaust conduit 113 near an outlet of an exhaust manifold 8 to oxidize unburned products such as HC and CO. Further, an NOx reduction catalyst 12 is disposed in the exhaust conduit downstream of a muffler 13. A mixer 10 is provided on the inlet side of the reduction catalyst 12 to evenly mix H<sub>2</sub> with exhaust gas.

An H<sub>2</sub> generator 11 (shown in enlarged detail in FIG. 7) includes an inner core in the form of a coiled tube 114 inserted in the exhaust conduit. At an inlet end 114a of the inner core, an electromagnetic fuel injection valve 115 is provided for injecting methanol fuel into the inner core. An outlet end 114b of the inner core leads to the mixer 10 through a conduit 116. As shown in FIG. 8, a porous ceramic member 117 for evaporating the methanol is located at the inlet of the inner core, and a reforming catalyst 14 in the form of pellets fills the inner core downstream of the methanol evaporating ceramic member. If the reforming catalyst is in monolithic form, the

inner core is changed from a coil to a straight tube. Pd is used for the reforming catalyst.

In FIG. 6, an intake air sensor 15 is installed in the intake conduit 118 to detect the amount of air supplied to the engine 112, and an NOx sensor 16 is installed in the exhaust conduit of the engine to detect the NOx concentration of the exhaust gas. In the one-liter engine example of FIG. 6, since the moles of H<sub>2</sub> required are equal to the moles of NOx, 0.3 l/min of H<sub>2</sub> is necessary at a vehicle speed of 50 Km/h and 1.0 l/min of H<sub>2</sub> is necessary when the engine is operated at the maximum output. The H<sub>2</sub> is produced by reforming a portion of the fuel. The portion of fuel consumed to produce the required H<sub>2</sub> is equal to or less than 1 - 2% of the fuel required to drive a vehicle. As an amount of 15 - 20% of fuel is saved by using a lean burn engine, the amount of 1 - 2% is negligible compared with the amount of 15 - 20%. Thus, the fuel economy of the lean burn engine is not degraded by adding an H<sub>2</sub> generator. In this connection, the amount of methanol required to generate the H<sub>2</sub> is about 0.15 l/min at a vehicle speed of 50 Km/h.

In the first embodiment of the invention, since only a small amount of fuel is reformed by the H<sub>2</sub> generator 11 and NOx is reduced through reaction with the generated H<sub>2</sub> at the NOx reduction catalyst 12 at low temperatures, the amount of NOx can be decreased independently of the excess air ratio of the engine 112. CO, which may be produced together with H<sub>2</sub>, can be transformed by the following reaction:



Further, CO can be separated from H<sub>2</sub> by a Pd membrane, and H<sub>2</sub> of high purity can be supplied into the inlet side of the NOx reduction catalyst 12. However, since the amount of produced CO is very small, CO acts as a reduction material in the NOx reduction catalyst 12. Thus, there is no fear that CO is exhausted to atmosphere.

FIG. 9 illustrates a second embodiment of the invention which comprises a natural gas engine 119 equipped with an H<sub>2</sub> generator 120 and used for an air conditioner or a power generator. Unlike a vehicle engine, such an engine is operated at a constant engine speed and a constant engine load. Therefore, it is easy to maintain constant temperatures of the reforming catalyst of the H<sub>2</sub> generator 120 and the NOx reduction catalyst 12. Since the structures of the apparatus of the second embodiment are substantially the same as those of the first embodiment, descriptions of them will be omitted.

The fuel supplied to the H<sub>2</sub> generator 120 is natural gas. The amount of natural gas and the amount of air are controlled by respective control valves 121 and 122, which are controlled in response to the same sensor outputs in substantially the same manner as in the first embodiment.

FIG. 10 illustrates an embodiment of an H<sub>2</sub> mixer and NOx reduction catalyst container according to the invention. NOx reduction characteristics are greatly

affected by the  $H_2$  supply conditions and structures. In FIG. 10, the engine exhaust gas including NOx and  $O_2$  flows through an exhaust conduit 65 to an NOx reduction catalytic converter 60, and  $H_2$  is supplied to an  $H_2$  mixer 69 located on the inlet side of the NOx reduction catalytic converter 60.

The NOx conversion characteristics for two types of catalyst structures are shown in FIG. 11, where the abscissa measures a ratio of the amount of supplied  $H_2$  to the amount of NOx, and the ordinate measures an NOx conversion or NOx purification rate. In a case where a catalyst in the form of pellets 61, as shown in FIG. 12, fill the NOx reduction catalytic converter 60 of FIG. 10, the NOx reduction catalyst produces a high NOx conversion, as shown in FIG. 11. In a case where a monolithic catalyst 62, as shown in FIG. 13, fills the catalytic converter of FIG. 10, FIG. 11 shows that the NOx conversion of the NOx reduction catalyst decreases, even if the amount of supplied  $H_2$  is the same.

This is because, in the case of the catalyst in the form of pellets,  $H_2$  and NOx are well mixed with each other when they flow through the labyrinthine clearances between the pellets. In contrast, in the case of the monolithic catalyst, since the monolithic catalyst has numerous parallel passages which are independent of each other, an uneven distribution of  $H_2$  at the inlet of the catalyst is maintained up to the outlet of the catalyst. Thus, the utilization rate of  $H_2$  of the monolithic catalyst is inferior to that of the pellet-type catalyst.

From the operational viewpoint of an engine exhaust system, however, the pellets of catalyst are apt to cause abrasion due to vibration and to get smaller in size. They also tend to cause a large flow friction loss due to the labyrinth passages and thus to raise the engine back pressure and to degrade the power characteristic of the engine. Therefore, it is desirable to use a monolithic catalyst for the NOx reduction catalyst.

If a monolithic catalyst is used in the NOx reduction catalytic converter, then a mixer 69 for evenly mixing  $H_2$  with NOx is necessary. FIGS. 14 and 15 illustrate a mixer 69 comprising an  $H_2$  injection nozzle 63. The  $H_2$  injection nozzle 63 is a pipe bent in the form of a letter L and has a plurality of radially directed injection holes 64. The number of injection holes 64 is preferably four to six in each of at least one plane perpendicular to the axis of the pipe (six holes in each of two mutually perpendicular planes are provided in the embodiment of FIGS. 14 and 15).

A ratio of an outside diameter  $d$  of the injection nozzle 63 to an inside diameter  $D$  of the exhaust conduit (exhaust pipe) 65 should be equal to or greater than 0.2 (20%). When the diameter  $d$  is increased relative to  $D$ , the flow resistance will be large, so that a portion of the exhaust pipe 65 may be enlarged in cross section, as shown in FIG. 16. A distance  $L$  (see FIG. 10) between the injection nozzle 63 and the NOx reduction catalyst 60 should be equal to or greater than twice the outside diameter  $D$  of a portion of the exhaust conduit not enlarged in cross section. Increasing  $L$  beyond ten times

$D$ , however, produces little additional effect in even mixing of  $H_2$  with NOx.

An alternative embodiment of the  $H_2$  mixer 69 is shown in FIGS. 17 and 18. In this embodiment, the mixer includes an HC injection nozzle 66 of a small diameter and a cylinder 68 having a diameter greater than that of the HC injection nozzle. The cylinder 68 has an open upstream end and an end plate at the downstream. A plurality of apertures 67 are formed in the wall of the cylinder 68. The  $H_2$  injected from the HC injection nozzle 66 mixes with a portion of the exhaust gas which enters the cylinder 68. The mixture of the  $H_2$  and the exhaust gas flows through the apertures of the cylinder 68 and mixes with the remaining portion of the exhaust gas flowing outside the cylinder 68. Mixing  $H_2$  with the exhaust gas in two steps produces a uniform mixture.

The mixing degree of  $H_2$  with exhaust gas is affected by the relative diameters of the nozzle 66 and the cylinder 68. Preferably, a ratio of the inside diameter  $D$  of the cylinder 68 to the outside diameter  $d$  of the injection nozzle 66 is in the range of 1.7 - 3, and most preferably 2, from the viewpoint of mixing.

Since the  $H_2$  mixing apparatus of the embodiment of FIGS. 17 and 18 having the above-defined ratio of  $D/d$  has a good mixing characteristic, the NOx reduction catalyst shows a high NOx conversion even if the NOx reduction catalytic converter has a monolithic catalyst. Since the required amount of  $H_2$  can be reduced by 30 - 60% at the same NOx conversion rate when the mixer is provided, the amount of fuel required to generate  $H_2$  can be decreased so that reduction in fuel economy is minimized when using a monolithic NOx reduction catalyst.

For example, the effect of the mixer was evaluated using a lean burn gasoline engine of 1.6 liters. In the tests, the engine speed was 2000 rpm, the torque was 40 Nm, and the NOx exhaust amount was 0.44 l/min. Without an  $H_2$  mixer, the  $H_2$  amount required to purify the NOx was 0.661 min, and the amount of fuel (methanol) to generate the  $H_2$  was 0.33 l/min.

When the mixer of FIGS 17 and 18 with the ratio  $D/d$  of 2 was used, the amount of  $H_2$  was 0.44 l/min, and the amount of fuel to generate the  $H_2$  was 0.22 l/min. Therefore, the amount of 0.11 l/min of fuel could be saved as compared with the above-described case having no mixer.

FIGS. 20 and 21 illustrate another embodiment of an  $H_2$  mixer and NOx catalytic converter wherein a lean NOx catalyst 82 is disposed in or near a muffler 80. When the NOx reduction catalyst is disposed in or near a muffler, where the exhaust gas temperature is low, the reaction rate of  $H_2$  with NOx is not high. So, the NOx reduction catalyst should be used at SV values (a ratio of the volume of exhaust gas passing through the catalyst to the volume of the catalyst) of 10,000 - 60,000, which are smaller than the SV values of 50,000 - 100,000 of the conventional catalyst disposed near the exhaust manifold. This means that the required volume of the NOx

reduction catalyst becomes greater than that of the conventional catalyst disposed near the exhaust manifold.

To make installation of the NOx reduction catalyst easy, the NOx reduction catalyst 82 and the muffler 80 are integrated as a single assembly 83 in the embodiment of FIGS. 20 and 21, wherein the lean NOx catalyst 82 is disposed in the exhaust muffler 80 so that the assembly 83 of the NOx reduction catalyst (Pt-zeolite catalyst) and the exhaust muffler is made compact.

Exhaust gas mixed with H<sub>2</sub> flows to the integral assembly 83 of the catalyst and muffler. The exhaust gas mixed with H<sub>2</sub> collides with a mixing plate 84 which has many apertures 85 of different sizes. When the exhaust gas mixed with H<sub>2</sub> flows through the apertures 85, the exhaust gas and H<sub>2</sub> mix well with each other. Then the mixed gas flows to the monolithic catalyst 82. Since no aperture is provided at a center portion of the mixing plate 84, the exhaust gas will not concentrate in a central portion of the monolithic catalyst 82. Since the sizes of the apertures 85 are different from each other, the speeds of portions of gas passing through the apertures are different so that the portions of gas are agitated and the sound is muffled due to interference between portions of the gas.

Since the muffler is usually disposed at a tail pipe of the exhaust conduit and the exhaust gas has been cooled before flowing to the muffler, the temperature of the gas entering the muffler is about 150 - 200°C at the maximum, and about 100 - 150°C in normal operations.

In the cases of the conventional three-way catalyst and the conventional Cu/zeolite-type lean NOx catalyst reducing NOx in the presence of HC, since these catalysts can show activity only in a temperature range above 300 - 400°C, they are not allowed to be disposed in a tailpipe muffler. As discussed above, however, when NOx reduction is effected by H<sub>2</sub> instead of by HC, NOx purification at low temperatures is possible. However, even in those cases, the temperature is in the range of 150 - 300°C and is slightly higher than the inlet temperature of the exhaust muffler.

It was experimentally investigated from the viewpoint of catalyst activity what kinds of catalysts should be used. From the experiments, it was found that Pd and Rh showed no activity, Cu showed a low activity, and Pt showed a high activity to reduce NOx in cooperation with H<sub>2</sub>. However, it was also found that Pt should be highly distributed and that, for the high distribution, a carrier having a high specific surface area (greater than 100 m<sup>2</sup>/g) such as zeolite was necessary.

Further, it was investigated whether the exhaust gas should be pretreated before mixing with H<sub>2</sub>. The experiment results are shown in FIG. 19. More particularly, when exhaust gas with no pretreatment was mixed with H<sub>2</sub> and the mixture was then introduced to the lean NOx catalyst (Pt catalyst), the lean NOx catalyst exhibited its peak activity at about 250°C, as shown by characteristic curve B in FIG. 19. On the other hand, if an oxidizing device such as an afterburner, a reactor, a three-way catalyst, or an oxidation catalyst was installed in the vicinity

of the engine exhaust manifold, when exhaust gas was caused to flow through the oxidizing device so that CO and HC were removed from the exhaust gas, the lean NOx catalyst showed its peak activity at 100 - 150°C, as shown by characteristic curve A in FIG. 19.

This temperature range of 100 - 150°C coincides with the inlet temperature of the exhaust muffler, which means that it is possible to install the Pt/zeolite-type NOx reduction catalyst 82 within the exhaust muffler 80. Further, it was found that it would be better to remove HC and CO from the exhaust gas before the exhaust gas reached the NOx reduction catalyst. This is because NOx conversion by the lean NOx catalyst would be improved if no soot resulting from incomplete burning of HC were formed on the catalyst.

Further, the sound muffling effect is improved by installing an interference tube EX1 at a location downstream of the monolithic converter 82.

An H<sub>2</sub> mixing and NOx reduction catalytic converter apparatus of FIG. 22 is different from the apparatus of FIGS. 20 and 21 only in the structure of the mixer. More particularly, the mixer of FIG. 22 comprises a mixing pipe 86 having a plurality of apertures 85, while the mixer of FIGS. 20 and 21 comprises a mixing plate. H<sub>2</sub> from an H<sub>2</sub> generator is injected into the mixing pipe. The apparatus of FIG. 22 has the same functions and advantages as those of the apparatus of FIGS. 20 and 21.

In the embodiments of FIGS. 20 & 21 and of FIG. 22, since the NOx reduction catalytic converter and the exhaust muffler are integrated into a single assembly 83, the assembly is compact and is easy to be mounted to a vehicle. Further, the apparatus maintains a high NOx conversion characteristic over the entire engine operation range.

## Claims

1. An NOx decreasing apparatus for an internal combustion engine comprising
  - an internal combustion engine (100) capable of fuel combustion at lean air-fuel ratios, the engine having an exhaust conduit (101), an upstream end of which is connected to the engine (100), and an exhaust muffler (3) installed in the exhaust conduit;
  - an NOx reduction catalyst (2) installed at a downstream, low temperature location in the exhaust conduit (101), the NOx reduction catalyst (2) being a Pt/zeolite catalyst capable of causing H<sub>2</sub> to selectively react with NOx at temperatures lower than 300°C under a predetermined engine running condition, wherein the predetermined engine running condition includes an excess oxygen condition, to thereby decompose the NOx into N<sub>2</sub> and H<sub>2</sub>O;
  - an H<sub>2</sub> generator (102) for generating H<sub>2</sub>, the H<sub>2</sub> generator (102) including an inner core inserted in the exhaust conduit at a location upstream of the muffler (3) and the NOx reduction catalyst (2) (101) and a reforming catalyst (1) for reforming fuel to generate H<sub>2</sub> housed in the inner core; and

- means (107) for supplying the generated H<sub>2</sub> adjacent to the inlet of the NO<sub>x</sub> reduction catalyst (2), wherein the means (107) for supplying the generated H<sub>2</sub> comprises a mixer (10) for mixing H<sub>2</sub> with exhaust gas from the engine, wherein the mixer (1) is located in the exhaust conduit (101) adjacent to the inlet of the NO<sub>x</sub> reduction catalyst (2).
2. An apparatus according to Claim 1, wherein the H<sub>2</sub> generator (102) includes a reforming catalyst (1) for reforming methanol to generate H<sub>2</sub>.
  3. An apparatus according to Claim 2, wherein the reforming catalyst (1) includes at least one kind of catalyst metal selected from the group composed of noble metal including Pt and Pd and transition metal including Cu, Cr, and Ni, so that said methanol can be evaporated by heat from exhaust gas and reformed at the reforming catalyst (1) at about 300°C to generate H<sub>2</sub>.
  4. An apparatus according to Claim 2, wherein the reforming catalyst (1) comprises a Cu-Ni-Cr/alumina catalyst, so that said methanol can be evaporated by heat from exhaust gas, mixed with air, and reformed at the reforming catalyst (1) at 400 - 500°C to generate H<sub>2</sub>.
  5. An apparatus according to Claim 2, wherein the reforming catalyst (1) includes either one of Cu-Mn and Cu-Zn, so that said methanol can be added with at least one of water vapor, air and mixture of methanol and water, and reformed at the reforming catalyst at about 250°C to generate H<sub>2</sub>.
  6. An apparatus according to Claim 1, wherein the H<sub>2</sub> generator (102) includes a reforming catalyst (1) for reforming hydrocarbons such as LPG and natural gas to generate H<sub>2</sub>.
  7. An apparatus according to Claim 6, wherein the reforming catalyst (1) includes at least one kind of metal selected from the group composed of Ni, Co and Rh, so that said hydrocarbons can be added with at least one of water vapor, air and water, and reformed at the reforming catalyst at 300 - 800°C to generate H<sub>2</sub>.
  8. An apparatus according to Claim 1, wherein the engine (100) is a hydrogen engine, and the H<sub>2</sub> generator (102) comprises an H<sub>2</sub> fuel tank for the engine.
  9. An apparatus according to Claim 1, further comprising
    - an NO<sub>x</sub> sensor (6) for detecting an NO<sub>x</sub> concentration of exhaust gas to generate an output;
    - an intake air sensor (5) for detecting a volume flow of intake air to generate an output; and
  - a controller (7) for determining an amount of NO<sub>x</sub> included in exhaust gas from the engine based on the outputs of the NO<sub>x</sub> sensor and the intake air sensor, and determining an amount of H<sub>2</sub> required to reduce the determined amount of NO<sub>x</sub>.
  10. An apparatus according to Claim 1, further comprising
    - engine operating condition detecting sensors for detecting engine operating conditions and generating output, the engine operating condition detecting sensors including an engine speed sensor and an engine load sensor;
    - a controller for determining an amount of NO<sub>x</sub> included in exhaust gas from the engine based on the outputs from the engine operating condition detecting sensors, and determining an amount of H<sub>2</sub> required to reduce the determined amount of NO<sub>x</sub>.
  11. An apparatus according to Claim 1, further comprising
    - an oxidizing device (9) located in the exhaust gas conduit upstream of the NO<sub>x</sub> reduction catalyst for oxidizing HC and CO included in exhaust gas from the engine, and wherein the engine has an exhaust manifold having an outlet, the H<sub>2</sub> generator (11) being disposed at the outlet of the exhaust manifold, and the NO<sub>x</sub> reduction catalyst (12) being located in the muffler or a portion of the exhaust conduit downstream of the muffler (13).
  12. An apparatus according to claim 1, further comprising an oxidizing device (9) for oxidizing HC and CO included in exhaust gas from the engine, and wherein the NO<sub>x</sub> reduction catalyst (12) is a Pt type catalyst which comprises platinum deposited on a carrier consisting of zeolite.
  13. An apparatus according to claim 12, wherein the Pt type catalyst of the NO<sub>x</sub> reduction catalyst (82) is housed in the muffler (80) to constitute a single assembly of the NO<sub>x</sub> reduction catalyst and the muffler.
  14. An apparatus according to Claim 1, wherein inner core of the H<sub>2</sub> generator (102) is constructed of a coiled tube (114), and wherein the H<sub>2</sub> generator (102) further includes an electro-magnetic injection valve (115) for injecting methanol into one end portion.
  15. An apparatus according to claim 1, wherein the NO<sub>x</sub> reduction catalyst (2) comprises a pellet type catalyst (61).
  16. An apparatus according to claim 1, wherein the NO<sub>x</sub> reduction catalyst (2) comprises a monolithic type catalyst (62), and wherein the mixer (10, 69) comprises an injection nozzle (63) connected to the H<sub>2</sub>

generator and having a plurality of radially directed holes (64) for injecting H<sub>2</sub> therethrough.

17. An apparatus according to claim 16, wherein the injection nozzle (63) has an outside diameter equal to or greater than 20% of an inside diameter of the exhaust conduit (65), the exhaust conduit being enlarged in diameter at a portion in which the injection nozzle is disposed, the injection nozzle (63) being spaced apart from the NO<sub>x</sub> reduction catalyst (60) by a distance at least twice the inside diameter of the exhaust conduit (65) and no more than ten times the inside diameter of the exhaust conduit (65). 5
18. An apparatus according to claim 1, wherein the NO<sub>x</sub> reduction catalyst (2) comprises a monolithic type catalyst (62), and wherein the mixer (10) comprises an injection nozzle (66) having a first diameter, and a cylinder (68) coaxial with and downstream of the injection nozzle (66), the cylinder (68) having a second diameter greater than the first diameter and having a plurality of injection apertures (67) formed in a wall of the cylinder. 10
19. An apparatus according to claim 18, wherein a ratio of the second diameter to the first diameter is in the range of 1.7 to 3. 15
20. An apparatus according to claim 19, wherein the ratio of the second diameter to the first diameter is substantially 2. 20
21. An apparatus according to claim 13, further comprising a mixing plate (84) disposed in the muffler (80) and upstream of the NO<sub>x</sub> reduction catalyst (82), the mixing plate (84) comprising a plate having apertures (85) of different sizes. 25
22. An apparatus according to claim 13, wherein the means for supplying the generated H<sub>2</sub> comprises a mixing pipe (86) disposed in the muffler and connected to the exhaust conduit, the mixing pipe (86) having apertures (85) formed in a wall of the mixing pipe (86), the H<sub>2</sub> generator injecting the generated H<sub>2</sub> into the mixing pipe (86). 30
23. An apparatus according to claim 12, wherein the oxidizing device is any one of an afterburner, a reactor, a three-way catalyst, and an oxidation catalyst. 35

#### Patentansprüche

1. Einrichtung zur Verminderung von Stickstoffoxiden bzw. NO<sub>x</sub> für eine Brennkraftmaschine, die aufweist: 40
  - eine Brennkraftmaschine (100), ausgelegt zum Verbrennen vom Kraftstoff bei mageren

Luft/Kraftstoff-Verhältnissen, wobei die Brennkraftmaschine aufweist:

- eine Abgasleitung (101),
  - ein zustromseitiges Ende, welches mit der Brennkraftmaschine (100) verbunden ist, und
  - einen Auspufftopf (3), der in der Abgasleitung angeordnet ist,
  - einen NO<sub>x</sub>-Reduktionskatalysator (2), der an einer abstromseitigen Niedrigtemperatur-Position in der Abgasleitung (101) angeordnet ist, der NO<sub>x</sub>-Reduktionskatalysator (2) ein Pt/Zeo-lith-Katalysator ist, der in der Lage ist, ein selektives Reagieren von H<sub>2</sub> mit NO<sub>x</sub> bei Temperaturen von weniger als 300°C unter einer vorbestimmten Laufbedingung der Brennkraftmaschine zu bewirken, wobei die vorbestimmte Laufbedingung der Brennkraftmaschine eine Überschuß-Sauerstoff-Bedingung aufweist, um dadurch die NO<sub>x</sub> in N<sub>2</sub> und H<sub>2</sub>O zu zerlegen,
  - einen H<sub>2</sub>-Erzeuger (102) zum Erzeugen von H<sub>2</sub>, wobei der H<sub>2</sub>-Erzeuger (102) einen Innenkern aufweist, der in der Abgas-Leitung (101) an einer Position zustromseitig des Auspufftopfs (3) und des NO<sub>x</sub>-Reduktionskatalysators (2) angeordnet ist, und einen Reformkatalysator (1) zum Reformieren von Kraftstoff zum Erzeugen von H<sub>2</sub>, angeordnet im Innenkern, und
  - eine Vorrichtung (107) zum Zuführen des erzeugten H<sub>2</sub> neben dem Einlaß des NO<sub>x</sub>-Reduktionskatalysators (2), wobei die Vorrichtung (107) zum Zuführen des erzeugten H<sub>2</sub> einen H<sub>2</sub>-Mischer (10) zum Vermischen des H<sub>2</sub> mit dem Abgas aus der Brennkraftmaschine aufweist, wobei der H<sub>2</sub>-Mischer (10) in der Abgasleitung (101) neben dem Einlaß des NO<sub>x</sub>-Reduktionskatalysators (2) angeordnet ist.
2. Einrichtung nach Anspruch 1, wobei der H<sub>2</sub>-Erzeuger (102) einen Reformkatalysator (1) zum Erzeugen von H<sub>2</sub> durch Reformieren von Methanol aufweist.
  3. Einrichtung nach Anspruch 2, wobei der Reformkatalysator (1) mindestens eine Katalysatormetalart aufweist, ausgewählt aus der Gruppe, welche Edelmetall aufweist, einschließlich Pt und Pd, und Übergangsmetalle aufweist, einschließlich Cu, Cr und Ni, so daß Methanol durch die Abgaswärme verdampft und zum Erzeugen von H<sub>2</sub> am Reformkatalysator (1) bei etwa 300°C reformiert werden kann.
  4. Einrichtung nach Anspruch 2, wobei der Reformkatalysator (1) einen Cu-Ni-Cr/Tonerde-Katalysator aufweist, so daß zum Erzeugen von H<sub>2</sub> Methanol durch die Abgaswärme verdampft, mit Luft vermischt und am Reformkatalysator (1) bei 400 - 500°C reformiert werden kann.

5. Einrichtung nach Anspruch 2, wobei der Reformkatalysator (1) jeweils entweder Cu-Mn oder Cu-Zn aufweist, so daß zum Erzeugen von H<sub>2</sub> Methanol mindestens entweder Wasserdampf oder Luft oder eine Gemisch aus Methanol und Wasser hinzugefügt werden kann, wobei das Gemisch am Reformkatalysator bei etwa 250°C reformiert wird. 5
6. Einrichtung nach Anspruch 1, wobei der H<sub>2</sub>-Erzeuger (102) zum Erzeugen von H<sub>2</sub> einen Reformkatalysator (1) zum Reformieren von Kohlenwasserstoffen, wie z. B. VEG bzw. verflüssigtes Erdölgas und Erdgas, aufweist. 10
7. Einrichtung nach Anspruch 6, wobei der Reformkatalysator (1) 15
- mindestens ein Metallelement aufweist, ausgewählt aus der Gruppe, die Ni, Co und Rh aufweist, so daß den Kohlenwasserstoffen mindestens entweder Wasserdampf oder Luft oder Wasser hinzugefügt werden kann, und das Reformieren am Reformkatalysator bei 300 - 800°C erfolgt, um H<sub>2</sub> zu erzeugen. 20
8. Einrichtung nach Anspruch 1, wobei die Brennkraftmaschine (100) eine Wasserstoff-Brennkraftmaschine ist und der H<sub>2</sub>-Erzeuger (102) einen H<sub>2</sub>-Brennstofftank für die Brennkraftmaschine aufweist. 25
9. Einrichtung nach Anspruch 1, die ferner aufweist: 30
- einen NO<sub>x</sub>-Sensor (6) zum Erfassen einer NO<sub>x</sub>-Konzentration des Abgases, um eine Ausgangsinformation zu erzeugen, 35
  - einen Ansaugluftsensor (5) zum Erfassen eines Ansaugluftvolumenstroms, um eine Ausgangsinformation zu erzeugen, und
  - eine Steuervorrichtung (7) zum Bestimmen einer NO<sub>x</sub>-Menge, die im Abgas der Brennkraftmaschine enthalten ist, basierend auf den Ausgangsinformationen des NO<sub>x</sub>-Sensors und des Ansaugluftsensoren, und Bestimmen einer H<sub>2</sub>-Menge, die zum Vermindern der bestimmten NO<sub>x</sub>-Menge erforderlich ist. 40
10. Einrichtung nach Anspruch 1, die ferner aufweist: 45
- Brennkraftmaschinen-Betriebsbedingungserfassungssensoren zum Erfassen der Brennkraftmaschinen-Betriebsbedingungen und Erzeugen einer Ausgangsinformation, wobei die Brennkraftmaschinen-Betriebsbedingungserfassungssensoren einen Brennkraftmaschinen-Drehzahlsensor und einen Brennkraftmaschinen-Belastungssensor aufweisen, 50
  - eine Steuervorrichtung zum Bestimmen einer NO<sub>x</sub>-Menge, die im Abgas der Brennkraftmas-

chine enthalten ist, basierend auf den Ausgangsinformationen der Brennkraftmaschinen-Betriebsbedingungserfassungssensoren, und Bestimmen einer für das Reduzieren der bestimmten NO<sub>x</sub>-Menge erforderlichen H<sub>2</sub>-Menge.

11. Einrichtung nach Anspruch 1, die ferner aufweist:

- eine Oxydiervorrichtung (9), die zustromseitig des NO<sub>x</sub>-Reduktionskatalysators in der Abgasleitung angeordnet ist, zum Oxydieren des im Abgas der Brennkraftmaschine enthaltenen KW und CO bzw. Kohlenmonoxid, und wobei die Brennkraftmaschine einen Auspuffkrümmer mit einem Auslaß aufweist, der H<sub>2</sub>-Erzeuger (11) am Auslaß des Auspuffkrümmers angeordnet ist und der NO<sub>x</sub>-Reduktionskatalysator (12) im Auspufftopf oder in einem Abschnitt der Abgasleitung abstromseitig des Auspufftopfs (13) angeordnet ist.

12. Einrichtung nach Anspruch 1, die ferner aufweist:

- eine Oxydiervorrichtung (9) zum Oxydieren von im Abgas der Brennkraftmaschine enthaltenem KW und CO, und wobei der NO<sub>x</sub>-Reduktionskatalysator (12) ein Pt-Type-Katalysator ist, welcher Platin, auf einem Träger aus Zeolith angeordnet, aufweist.

13. Einrichtung nach Anspruch 12, wobei der Pt-Type-Katalysator des NO<sub>x</sub>-Reduktionskatalysators (82) im Auspufftopf (80) angeordnet ist, um eine einstückige Anordnung aus NO<sub>x</sub>-Reduktionskatalysator und Auspufftopf auszubilden. 35

14. Einrichtung nach Anspruch 1, wobei der Innenkern des H<sub>2</sub>-Erzeugers (102) als ein gewundenes Rohr (114) ausgebildet ist, und wobei der H<sub>2</sub>-Erzeuger (102) außerdem zum Einspritzen von Methanol in einen Endabschnitt ein elektromagnetisches Kraftstoffeinspritzventil (115) aufweist. 40

15. Einrichtung nach Anspruch 1, wobei der NO<sub>x</sub>-Reduktionskatalysator (2) einen Granulat-Type-Katalysator (61) aufweist. 45

16. Einrichtung nach Anspruch 1, wobei der NO<sub>x</sub>-Reduktionskatalysator (2) einen monolithischen Katalysator (62) aufweist, und wobei der H<sub>2</sub>-Mischer (10, 69) eine H<sub>2</sub>-Einspritzdüse (63) aufweist, die mit dem H<sub>2</sub>-Erzeuger verbunden ist und eine Vielzahl von radial gerichteten Einspritzlöchern (64) aufweist, um durch diese H<sub>2</sub> einzuspritzen. 50

17. Einrichtung nach Anspruch 16, wobei die H<sub>2</sub>-Einspritzdüse (63) einen Außendurchmesser gleich oder größer als 20% eines Innendurchmessers der Abgasleitung (65) aufweist, die Abgasleitung in 55

- einem Abschnitt, in welchem die H<sub>2</sub>-Einspritzdüse angeordnet ist, im Durchmesser vergrößert ist, die H<sub>2</sub>-Einspritzdüse (63) vom NO<sub>x</sub>-Reduktionskonverter (60) um eine Distanz beabstandet ist, die mindestens dem doppelten Innendurchmesser der Abgasleitung (65) und nicht mehr als dem zehnfachen Innendurchmesser der Abgasleitung (65) entspricht.
18. Einrichtung nach Anspruch 1, wobei der NO<sub>x</sub>-Reduktionskatalysator (2) einen monolithischen Katalysator (62) aufweist, und wobei der H<sub>2</sub>-Mischer (10) eine Einspritzdüse (66) aufweist, die einen ersten Durchmesser hat, und einen Zylinder (68) koaxial mit und abstromseitig der Einspritzdüse (66), der Zylinder (68) einen zweiten Durchmesser aufweist, der größer als der erste Durchmesser ist und eine Vielzahl von in einer Zylinderwand ausgebildeten Einspritzöffnungen (67) aufweist.
19. Einrichtung nach Anspruch 18, wobei ein Verhältnis des zweiten Durchmessers zum ersten Durchmesser im Bereich von 1,7 bis 3 ist.
20. Einrichtung nach Anspruch 19, wobei das Verhältnis des zweiten Durchmessers zum ersten Durchmesser im wesentlichen 2 ist.
21. Einrichtung nach Anspruch 13, die ferner eine im Auspufftopf (80) und zustromseitig des NO<sub>x</sub>-Reduktionskatalysators (82) angeordnete Mischplatte (84) aufweist und die Mischplatte (84) eine Platte mit Öffnungen (85) mit unterschiedlicher Größe aufweist.
22. Einrichtung nach Anspruch 13, wobei die Vorrichtung zum Bereitstellen des erzeugten H<sub>2</sub> ein im Auspufftopf angeordnetes und mit der Abgasleitung verbundenes Mischrohr (86) aufweist, das Mischrohr (86) in einer Wand des Mischrohres (86) ausgebildete Öffnungen (85) aufweist und der H<sub>2</sub>-Erzeuger das erzeugte H<sub>2</sub> in das Mischrohr (86) einspritzt.
23. Einrichtung nach Anspruch 12, wobei die Oxydiervorrichtung jeweils eine Nachverbrennvorrichtung oder ein Reaktor oder ein Drei-Weg-Katalysator oder ein Oxydationskatalysator ist.
- Revendications**
1. Dispositif pour diminuer l'émission de NO<sub>x</sub> des moteurs à combustion interne comprenant un moteur à combustion interne (100) capable de brûler un combustible avec des rapports air/combustible correspondant à des mélanges pauvres, le moteur comportant un conduit d'échappement (101), dont l'extrémité amont est connectée au moteur (100), et un pot silencieux d'échappement (3) installé dans le conduit d'échappement ;
- un catalyseur de réduction de l'émission de NO<sub>x</sub> (2) installé à un emplacement à basse température, en aval dans le conduit d'échappement (101), le catalyseur de réduction de l'émission de NO<sub>x</sub> (2) étant un catalyseur en zéolithe/Pt capable de faire réagir sélectivement H<sub>2</sub> avec NO<sub>x</sub> à des températures plus faibles que 300 °C sous une condition de régime de moteur prédéterminée, dans lequel la condition de régime de moteur prédéterminée inclut une condition d'excès en oxygène, afin de décomposer de ce fait le NO<sub>x</sub> en N<sub>2</sub> et H<sub>2</sub>O ;
- un générateur d'H<sub>2</sub> (102) destiné à générer H<sub>2</sub>, le générateur d'H<sub>2</sub> (102) comprenant un faisceau interne inséré dans le conduit d'échappement (101) à un emplacement situé en amont du pot d'échappement (3) et du catalyseur de réduction de l'émission de NO<sub>x</sub> (2), et un catalyseur de reformage (1) destiné à reformer le combustible afin de générer H<sub>2</sub>, logé dans le faisceau interne ; et
- des moyens (107) pour fournir l'H<sub>2</sub> généré, adjacents à l'entrée du catalyseur de réduction de l'émission de NO<sub>x</sub> (2), dans lequel les moyens (107) pour fournir l'H<sub>2</sub> généré comprennent un mélangeur (10) pour mélanger l'H<sub>2</sub> avec les gaz d'échappement provenant du moteur, dans lequel le mélangeur (10) est disposé dans le conduit d'échappement (101) adjacent à l'entrée du catalyseur de réduction de l'émission de NO<sub>x</sub> (2).
2. Dispositif selon la revendication 1, dans lequel le générateur d'H<sub>2</sub> (102) comprend un catalyseur de reformage (1) destiné à reformer du méthanol afin de générer H<sub>2</sub>.
3. Dispositif selon la revendication 2, dans lequel le catalyseur de reformage (1) comprend au moins une sorte de métal catalytique sélectionné parmi le groupe composé d'un métal noble comprenant le Pt et le Pd et un métal de transition comprenant le Cu, le Cr, et le Ni, de telle sorte que le dit méthanol puisse être évaporé par la chaleur provenant des gaz d'échappement puis reformé au contact du catalyseur de reformage (1) à environ 300 °C afin de générer H<sub>2</sub>.
4. Dispositif selon la revendication 2, dans lequel le catalyseur de reformage (1) comprend un catalyseur Cu-Ni-Cr/alumine, de telle sorte que le dit méthanol puisse être évaporé par la chaleur provenant des gaz d'échappement, mélangé à de l'air, puis reformé au contact du catalyseur de reformage (1) à environ 400 à 500 °C afin de générer H<sub>2</sub>.
5. Dispositif selon la revendication 2, dans lequel le catalyseur de reformage (1) comprend l'un des alliages Cu-Mn ou Cu-Zn, de telle sorte que le dit méthanol puisse être additionné d'au moins l'un des additifs comprenant de la vapeur d'eau, de l'air et un mélange de méthanol et d'eau, puis reformé au con-

tact du catalyseur de reformage (1) à environ 250 °C afin de générer H<sub>2</sub>.

6. Dispositif selon la revendication 1, dans lequel le générateur d'H<sub>2</sub> (102) comprend un catalyseur de reformage (1) destiné à reformer des hydrocarbures tels que GPL et gaz naturel afin de générer H<sub>2</sub>. 5
7. Dispositif selon la revendication 6, dans lequel le catalyseur de reformage (1) comprend au moins une sorte de métal sélectionné parmi le groupe composé du Ni, du Co et du Rh, de telle sorte que les dits hydrocarbures puissent être additionnés d'au moins l'un des additifs comprenant de la vapeur d'eau, de l'air et de l'eau, puis reformés au contact du catalyseur de reformage à environ 300 à 800 °C afin de générer H<sub>2</sub>. 10 15
8. Dispositif selon la revendication 1, dans lequel le moteur (100) est un moteur à hydrogène, et le générateur d'H<sub>2</sub> (102) comprend un réservoir à combustible H<sub>2</sub> pour le moteur. 20
9. Dispositif selon la revendication 1, comprenant de plus 25
  - une sonde à NO<sub>x</sub> (6) pour détecter la concentration de NO<sub>x</sub> dans les gaz d'échappement et engendrer un signal de sortie ;
  - un capteur d'air d'admission (5) pour détecter le flux volumique de l'air d'admission et engendrer un signal de sortie ;
  - un régulateur (7) qui détermine la quantité de NO<sub>x</sub> contenu dans les gaz d'échappement provenant du moteur, en se basant sur les signaux de sortie de la sonde à NO<sub>x</sub> et du capteur d'air d'admission, et qui détermine la quantité d'H<sub>2</sub> requise pour réduire la quantité déterminée de NO<sub>x</sub>. 30 35
10. Dispositif selon la revendication 1, comprenant de plus 40
  - des capteurs de détection des conditions de fonctionnement du moteur et générant des signaux de sortie, les capteurs de détection des conditions de fonctionnement du moteur comprenant un capteur de vitesse de rotation du moteur et un capteur de charge du moteur ;
  - un régulateur qui détermine la quantité de NO<sub>x</sub> contenu dans les gaz d'échappement provenant du moteur, en se basant sur les signaux de sortie des capteurs de détection des conditions de fonctionnement du moteur et qui détermine la quantité d'H<sub>2</sub> requise pour réduire la quantité déterminée de NO<sub>x</sub>. 45 50
11. Dispositif selon la revendication 1, comprenant de plus 55
  - un dispositif d'oxydation (9) placé dans le conduit d'échappement en amont du catalyseur de réduction de l'émission de NO<sub>x</sub>, pour oxyder les HC

et le CO contenus dans les gaz d'échappement provenant du moteur, et dans lequel le moteur comporte un collecteur d'échappement possédant une sortie, le générateur d'H<sub>2</sub> (11) étant disposé à la sortie du collecteur d'échappement, et le catalyseur de réduction de l'émission de NO<sub>x</sub> (12) étant placé dans le pot d'échappement ou dans une partie du conduit d'échappement située en aval du pot d'échappement (13).

12. Dispositif selon la revendication 1, comprenant de plus un dispositif d'oxydation (9) pour oxyder les HC et le CO contenus dans les gaz d'échappement provenant du moteur, et dans lequel le catalyseur de réduction de l'émission de NO<sub>x</sub> (12) est un catalyseur de type au Pt qui comprend du platine déposé sur un substrat porteur consistant en une zéolithe.
13. Dispositif selon la revendication 12, dans lequel le catalyseur de type au Pt du catalyseur de réduction de l'émission de NO<sub>x</sub> (82) est logé dans le pot d'échappement (80) afin de constituer un ensemble en un seul élément du catalyseur de réduction de NO<sub>x</sub> et du pot d'échappement.
14. Dispositif selon la revendication 1, dans lequel le faisceau interne du générateur d'H<sub>2</sub> (102) est construit en forme de serpentin (114), et dans lequel le générateur d'H<sub>2</sub> (102) comprend de plus une vanne d'injection électromagnétique (115) pour injecter du méthanol dans l'une de ses extrémités.
15. Dispositif selon la revendication 1, dans lequel le catalyseur de réduction de l'émission de NO<sub>x</sub> (2) comprend un catalyseur de type à granulés (61).
16. Dispositif selon la revendication 1, dans lequel le catalyseur de réduction de l'émission de NO<sub>x</sub> (2) comprend un catalyseur de type monolithique (62), et dans lequel le mélangeur (10, 69) comprend une buse d'injection (63) connectée au générateur d'H<sub>2</sub> et possédant une pluralité de trous d'injection orientés radialement (64) pour injecter l'H<sub>2</sub> à travers ces derniers.
17. Dispositif selon la revendication 16, dans lequel la buse d'injection (63) a un diamètre extérieur égal à ou plus grand que 20 % du diamètre intérieur du conduit d'échappement (65), le conduit d'échappement étant agrandi en diamètre au niveau d'une partie dans laquelle la buse d'injection est disposée, la buse d'injection (63) étant séparée du catalyseur de réduction de l'émission de NO<sub>x</sub> (60) d'une distance égale à au moins deux fois le diamètre intérieur du conduit d'échappement (65) et n'excédant pas plus de dix fois le diamètre intérieur du conduit d'échappement (65).

18. Dispositif selon la revendication 1, dans lequel le catalyseur de réduction de l'émission de  $\text{NO}_x$  (2) comprend un catalyseur de type monolithique (62), et dans lequel le mélangeur (10) comprend une buse d'injection (66) caractérisé par un premier diamètre, et un cylindre (68), coaxial avec, et placé en aval de la buse d'injection (66), le cylindre (68) ayant un second diamètre plus grand que le premier diamètre et possédant une pluralité d'ouvertures d'injection (67) pratiquées dans la paroi du cylindre.
19. Dispositif selon la revendication 18, dans lequel le rapport du second diamètre au premier diamètre se situe dans l'intervalle de 1,7 à 3.
20. Dispositif selon la revendication 19, dans lequel le rapport du second diamètre au premier diamètre vaut substantiellement 2.
21. Dispositif selon la revendication 13, comprenant de plus une plaque mélangeuse (84) disposée dans le pot d'échappement (80) et en amont du catalyseur de réduction de l'émission de  $\text{NO}_x$  (82), la plaque mélangeuse (84) comprenant une plaque comportant des ouvertures (85) de différentes tailles.
22. Dispositif selon la revendication 13, dans lequel le moyen de fourniture de l' $\text{H}_2$  généré comprend un tuyau mélangeur (86) placé dans le pot d'échappement et connecté au conduit d'échappement, le tuyau mélangeur (86) possédant des ouvertures (85) pratiquées dans la paroi du tuyau mélangeur (86), le générateur d' $\text{H}_2$  injectant l' $\text{H}_2$  généré dans le tuyau mélangeur (86).
23. Dispositif selon la revendication 12, dans lequel le dispositif d'oxydation est l'un quelconque d'un brûleur de post combustion, un réacteur, un catalyseur à trois voies, et un catalyseur d'oxydation.

5

10

15

20

25

30

35

40

45

50

55

FIG. 1

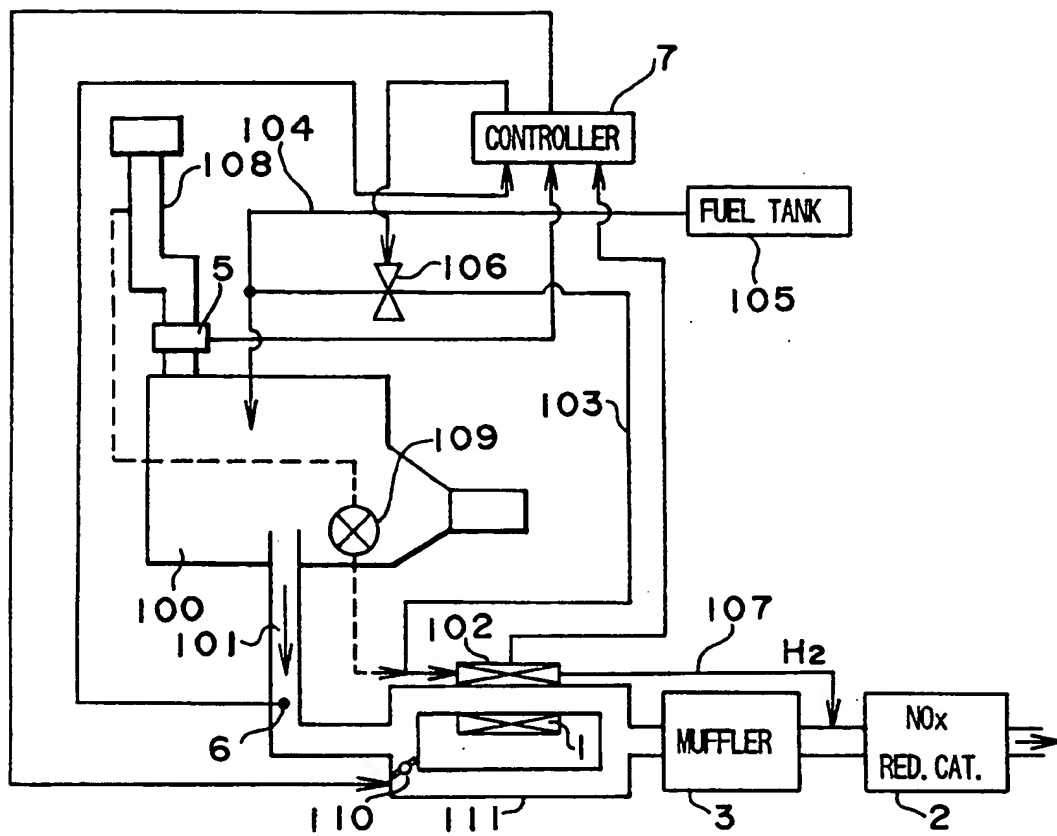


FIG. 2

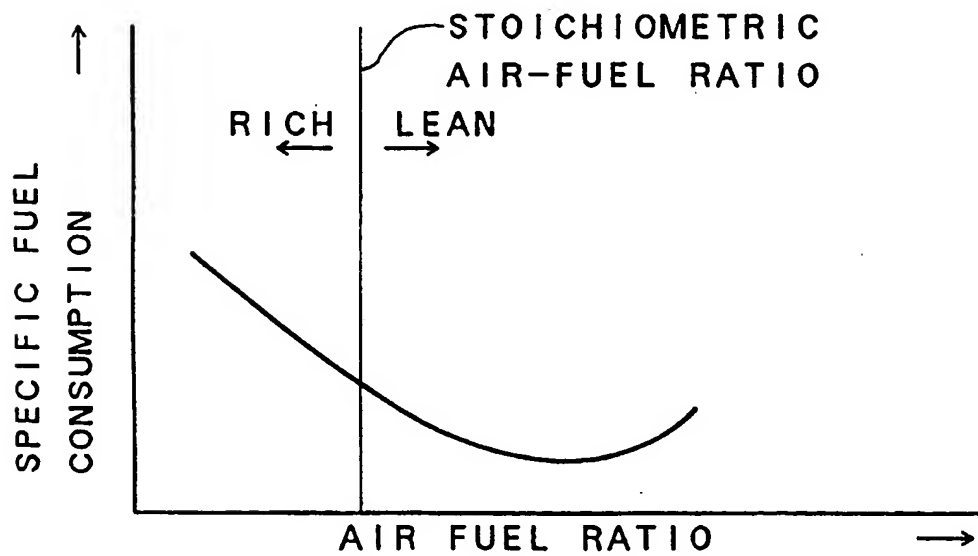


FIG. 3

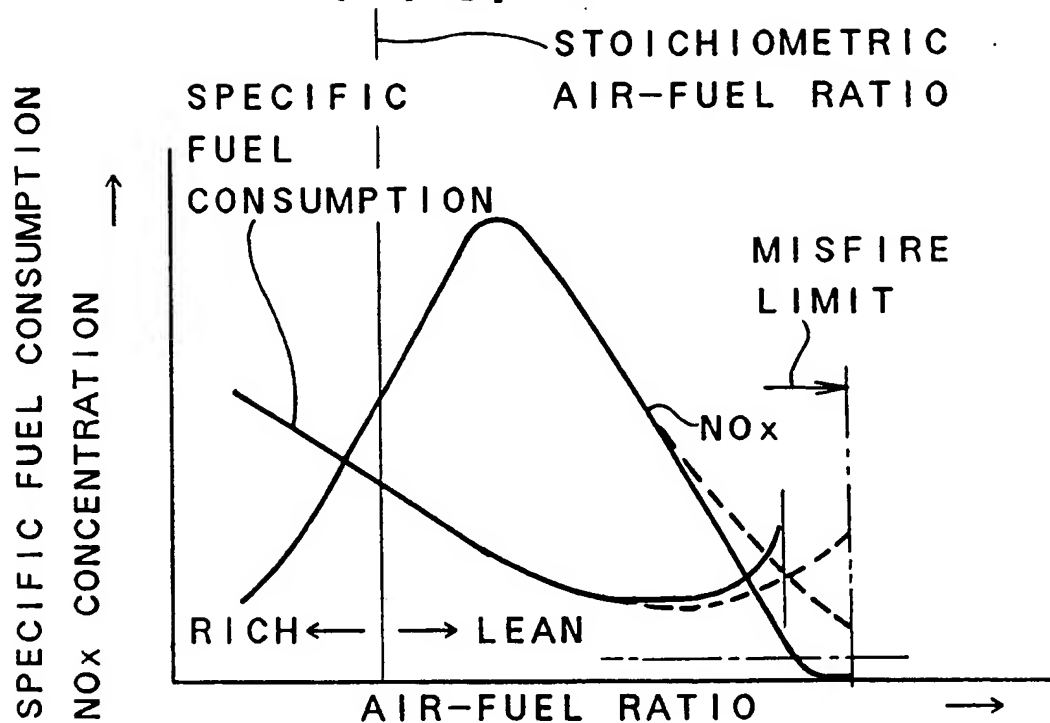


FIG. 4

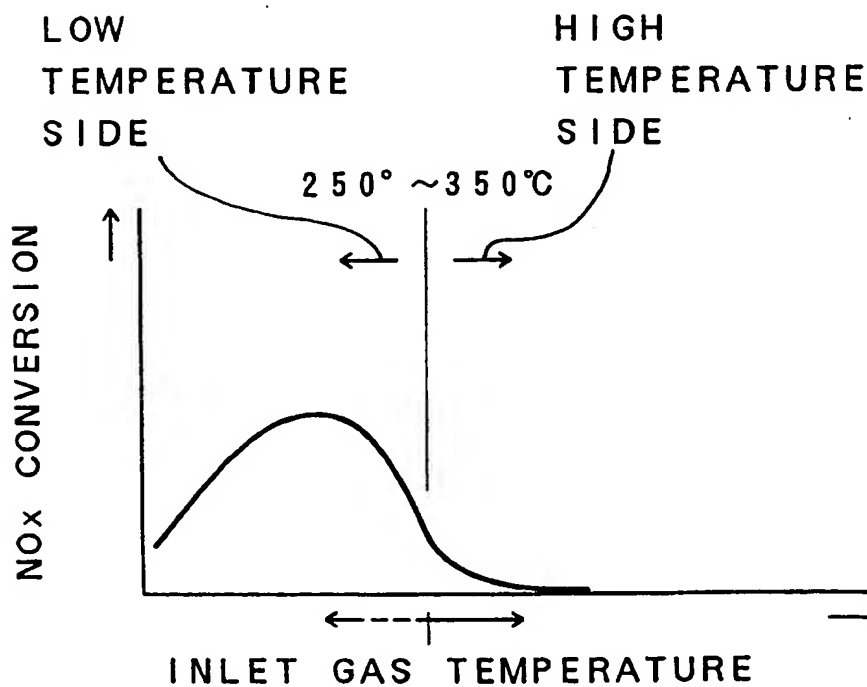


FIG. 5

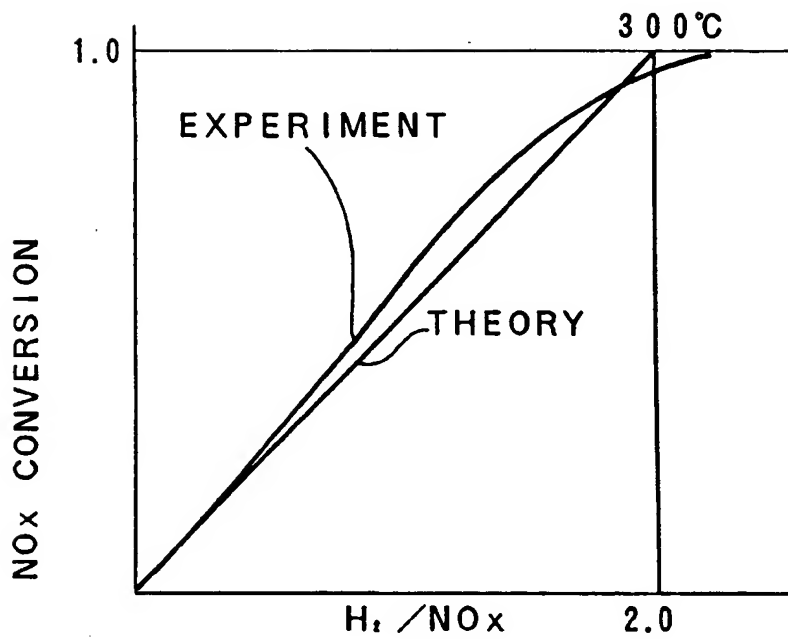


FIG. 6

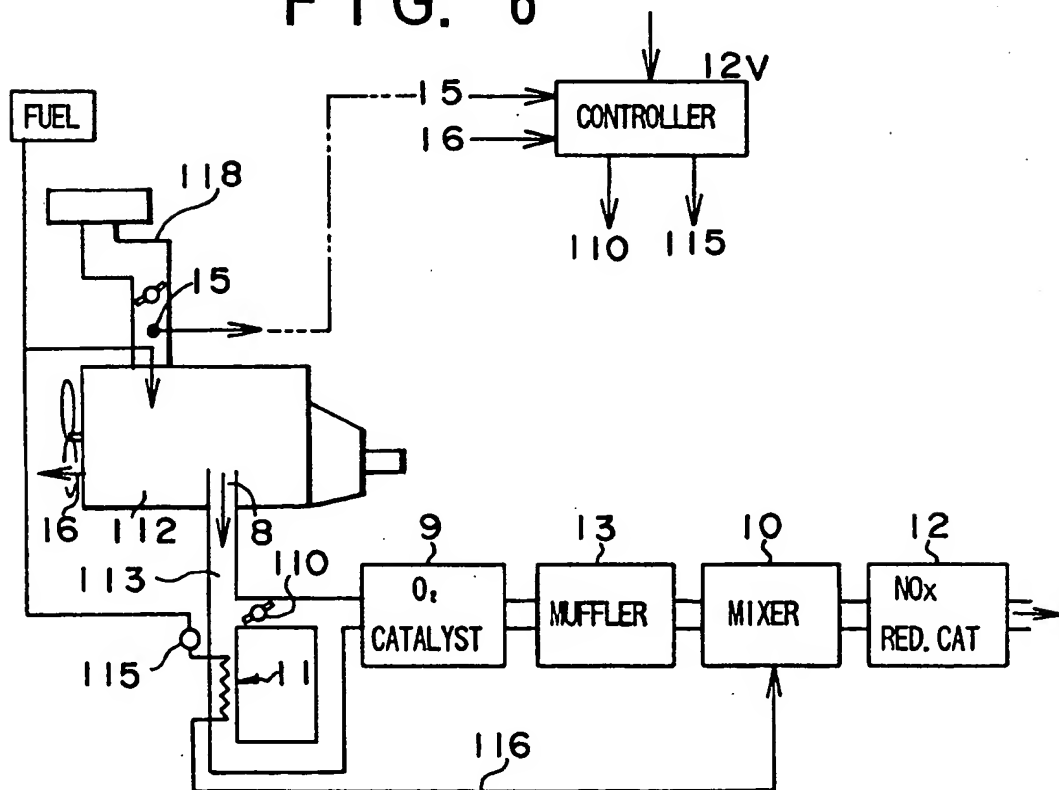


FIG. 7

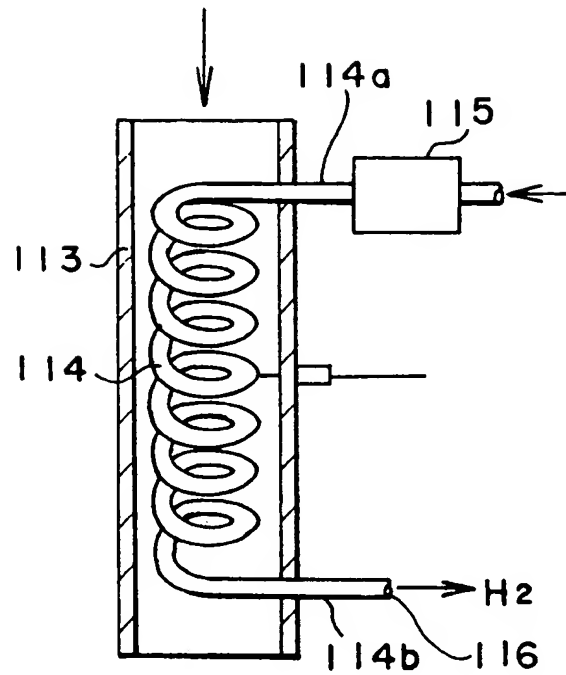


FIG. 8

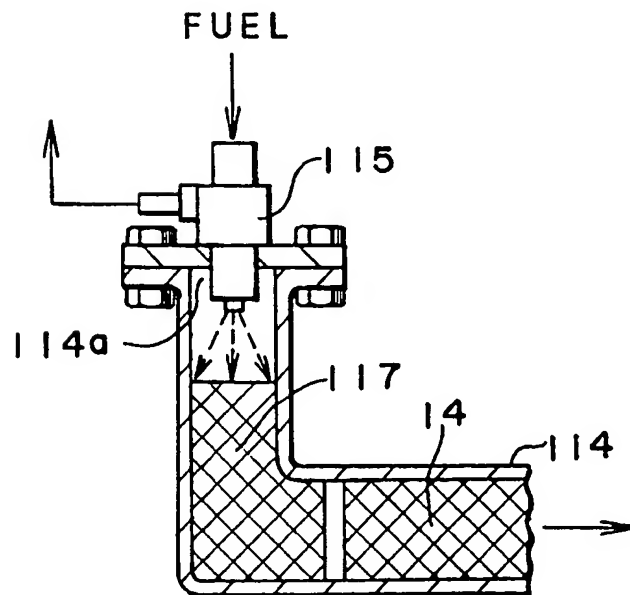


FIG. 9

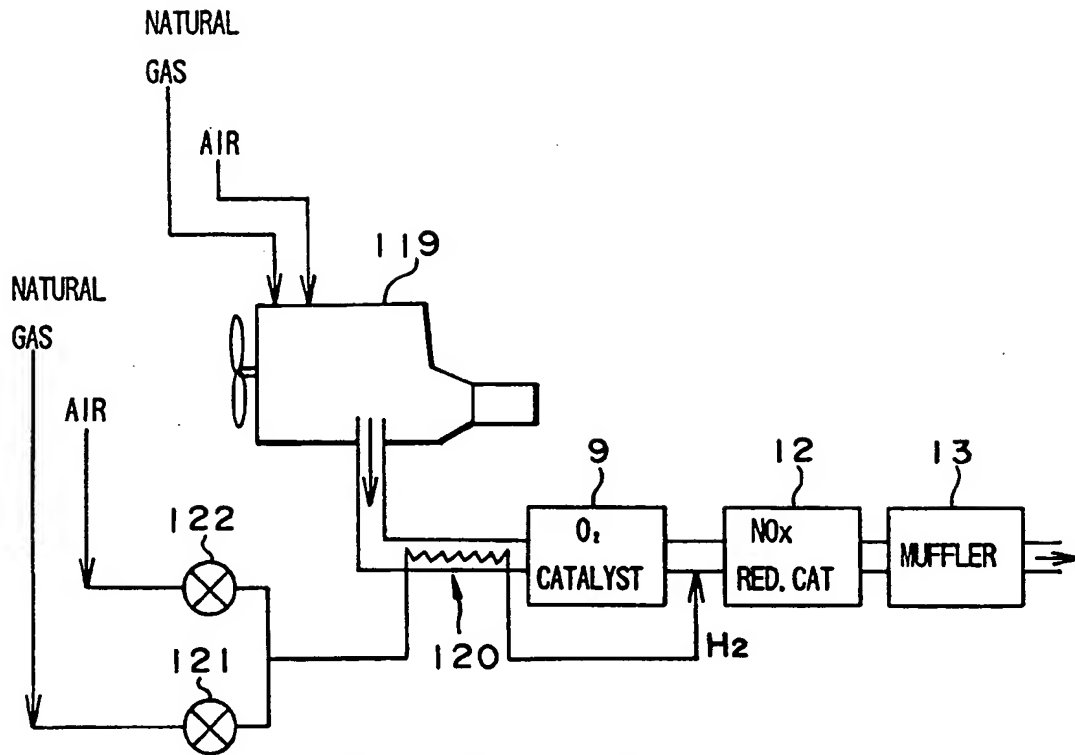


FIG. 10

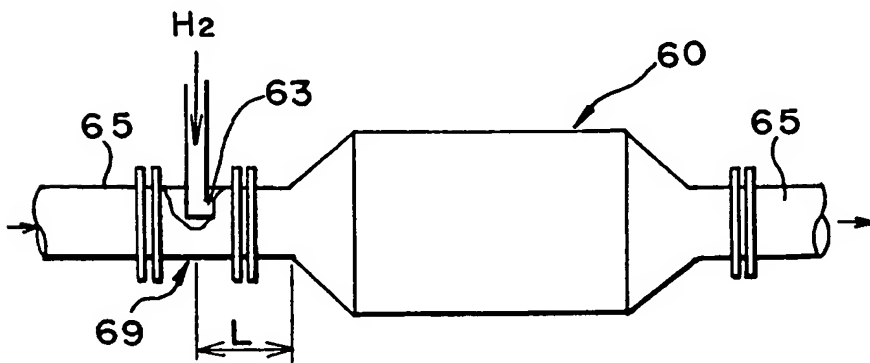


FIG. 11

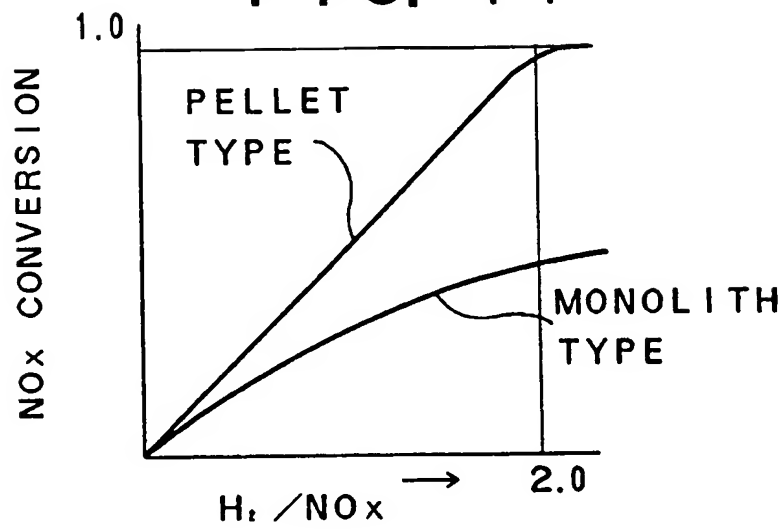


FIG. 12

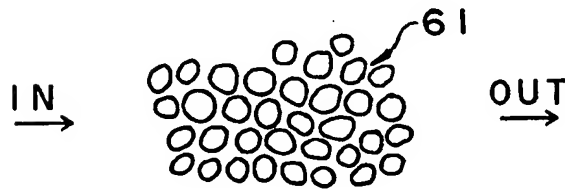


FIG. 13

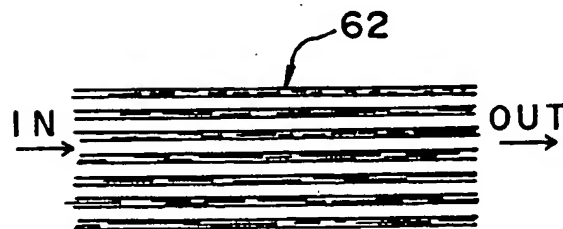


FIG. 14

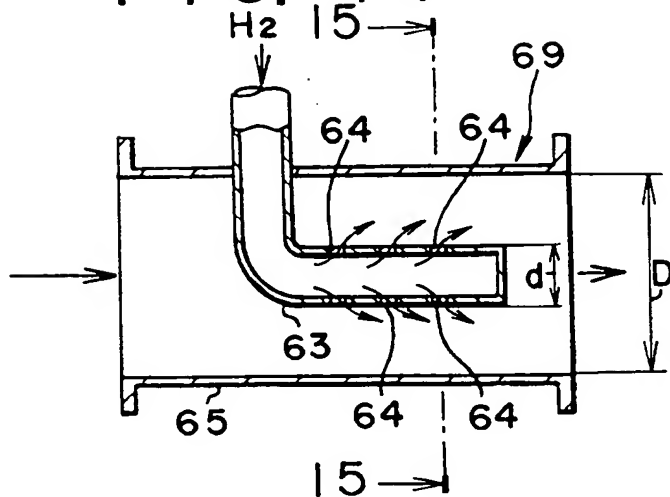


FIG. 15

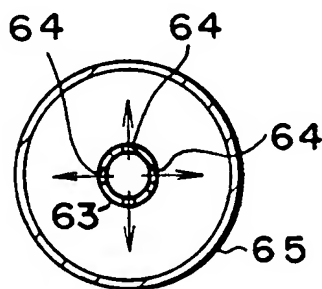


FIG. 16

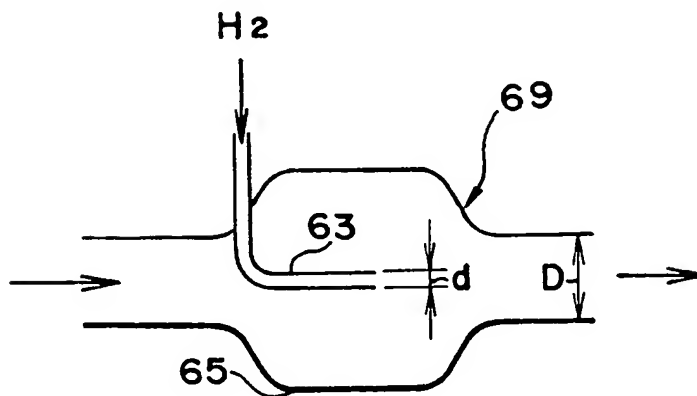


FIG. 17

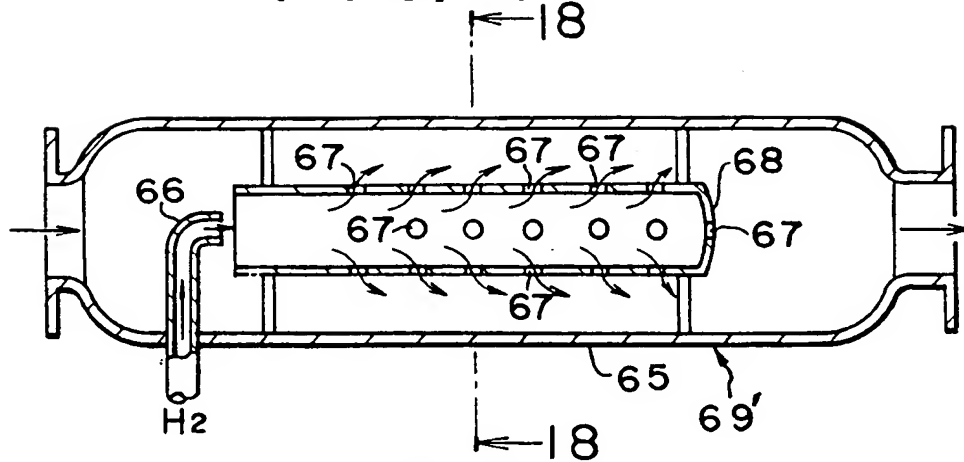


FIG. 18

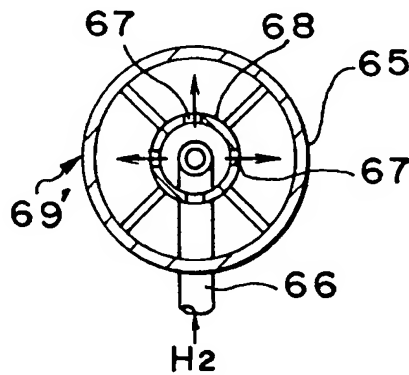
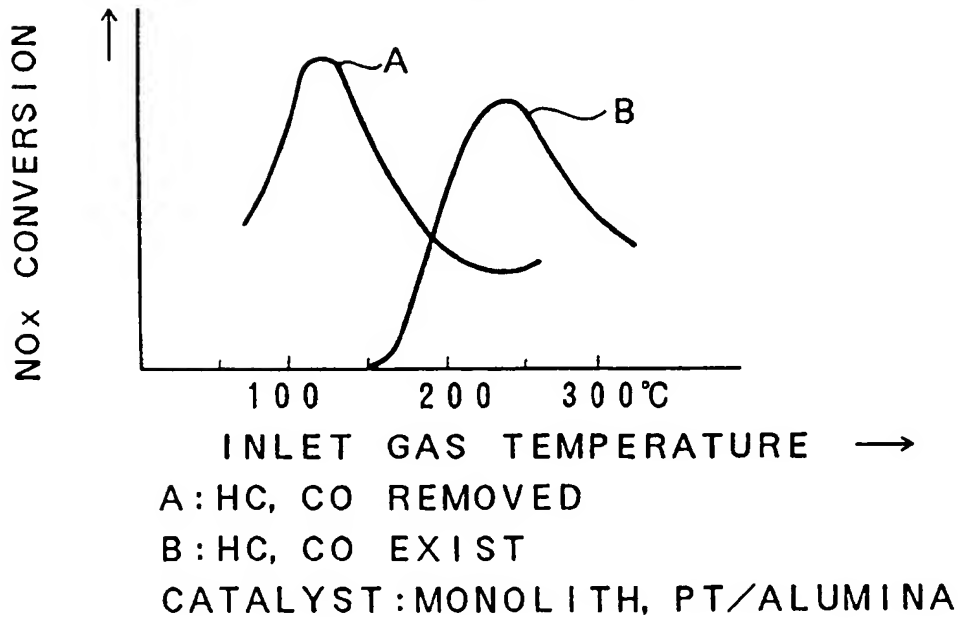
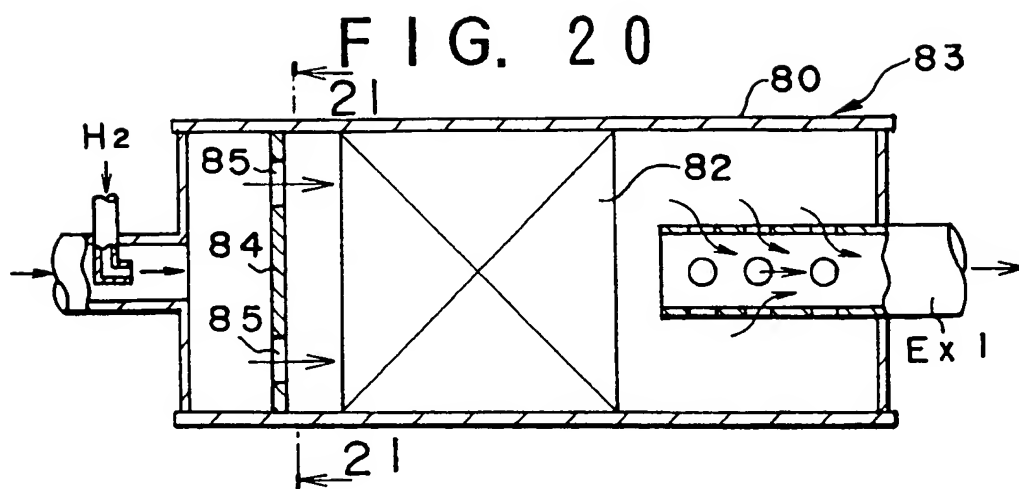
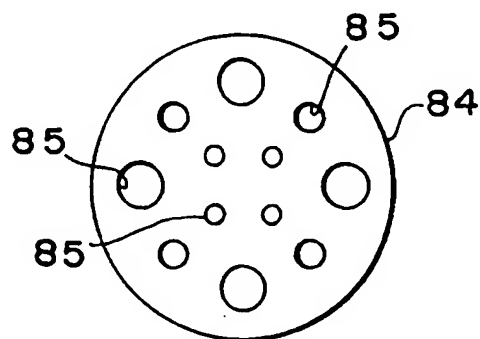


FIG. 19





**FIG. 21**



**FIG. 22**

